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THE FORCED CONVECTION FLOW OF $Ag - Al_2O_3$ HYBRIDNANOFLUID UNDER THE IMPACT OF EXOTHERMIC REACTION AND THERMAL RADIATION

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Abstract: The global huntfor more energy compelled the drive to develop substance with better heat transfer capacity and one major feat in this route is in nano science and technology. Here, the influence of both radiation and activation energy over a moving $Ag - Al_2O_3$ hybrid nanofluid being considered. The similarity solution to the governing problem was obtained and the numerical solution were obtained using a collocation method following a finite difference approach in MATLAB bvp4c solver. Effects of key parameter on fluid flow, heat and mass transfer rate were presented graphically and discussed.

Keywords: Exothermic reaction, hybrid nanofluid, forced convection, radiation.

1. Introduction

Fluid stream has different applications in many fields not confined to uses in oil extraction, engine cooling systems, circulation system in the body, drug targerting cleaning of soil from control, water fueled machines, fridges and climate control systems, hydroelectric plants. The mission for headway in each circle of life has required subject matter experts and analysts to foster groundbreaking thoughts and implant these in modern equipment and devices and gadgets utilized in the mechanical, electrical, everyday life and enterprises, for example, climate control systems, fridges, heat exchangers, electronic cooling, vehicle radiators, sun based warm, energy capacity, power through pressure framework and intensity pipes (Gul *et al.*, 2020). Straightforward fluids like water, oil, etc were prior being used for heat conduction and transfer, however it has been understood that this category of fluid have fallen underneath the new world's demand for energy transfer capability.

A huge achievement in energy issue with respect to nano content was kept in 1995 which can be credited to Choi (Choi, 1995). His examination and ensuing deals with what is today known as 'nanofluid' demonstrated that nanofluids relatively shows more warm limit and productivity for heat move rate than straightforward or convectional liquids. Choi and Eastman (1995) thought on improving heat conductivity of fluids with nanoparticles. The likely advantages of nanofluid with copper nanophase materials were talked about and one of such advantages is the drastic decrease in the heat exchanger siphoning power. Thermal vehicle in nanofluids was explored by Eastman *et al.*(2004). Afterward, a survey was made on nanofluid warm conductivity and their heat intensity upgrades by Yu *et al.* (2008). The exergy obliteration of constrained convective nanofluid through a channel with consistent wall temperature was examined by Rezaee and Tayebi (2010). The nuclear power stockpiling execution of Cu/paraffin nanofluids PCMs was mathematically reproduced by Shuying Wu *et al.*(2012). Loganathan *et al.* (2020) thought about the entropy investigation of third - order nanofluid stream on a permeable sheet. Later, the effect of slip on a two - stage stream of Newtonian nanofluid was explored by Ellahi *et al.* (2020).

In this era of constinuouslyevolving technology, another adaptation of nanofluid called hybrid nanofluid haverecently been developed. Research have shown that the hybrid nanofluid exhibit a higher heat transfer rate and more efficiency than the conventional nanofluids. Unlike the nanofluid, the hybrid nanofluid is

made up of more than one nanoparticle. The properties of hybrid nanofluid and its heat transfer marvel was explored by Suresh *et al.*(2012). Later, Nadeem *et al.* (2018) discussed the importance of hybrid nanofluid over simple nanofluids. The impacts of magnetic dipole on hybrid nanofluid flow wasconsidered by Gul *et al.* (2020). The flow of Cu-Al2O3 hybrid nanofluid fueled by a moving permeable surface was described by Aladdin *et al.*(2020). Rashidi *et al.* (2021) simulated the energy transfer of a hybrid nanosuspension within a heated chamber.

Combustion, heat packs, thermite reactions, manufacturing processes like production of cement, biological processes like respiration, firework and pyrotechnics are few out ofnumerous important chemical reactionfounded processes that involves the release of energy. This kind of chemical reaction which is known as exothermic reaction is characterized by products' energy being lower than the reactants' energy. However, a good understanding of exothermic reaction is essential for maximizing the products of exothermic reactions and based on this, researchers are endeared to investigate this kind of reaction.

A convection flow fueled by exothermic surface reaction was discussed by Chaudhary *et al.*(1995). Monica *et al.* (2017) examined the effects of exothermic reaction incompany of heat supply on stagnation point flow of a casson fluid.Koriko*et al.*(2017) investigated exothermic and endothermic reaction for a non-darcian micropolar fluid.The impact of exothermic reaction and viscous dissipation along a curved surface was explored by Ahmad *et al.* (2020). Shehu *et al.*(2022) analysed an exothermic fluid in an heated porous channel. Sharma *et al.*(2022) explored the entropy breeding for an endothermic/exothermic reaction in a mixed convective flow. The magnetic supported exothermic catalytic reaction along a curved surface was analysized by Muhammad Ashraf *et al.* (2022).

Propelled by every one of the above works, here we have endeavored a numerical examination because of an exothermic reaction and radiation on the constrained convection flow of an hybrid nanofluid with temperature subordinate fluid properties. Utilizing standard similarity variables, the overseeing conditions are changed into an arrangement of normal differential conditions. These acquired conditions are addressed mathematically utilizing matlab bvp5c. The outcomes acquired are introduced in tables and charts and conversations from there on made.



2. Mathematical Formulation

Consider a two-dimensional, steady, boundary layer stream of a hybrid nanofluid made up of $Ag - Al_2O_3$ hybrid nanoparticles with water base fluid past a half infinite plate moving in a uniformly free flow, U as shown in Fig.1. The system is such that the x-axis is allied to the plate surface while the

Based on the above assumptions together with ideas from previous works (AbdEl-Gaied and Hamad, 2013; Aladdin *et al.*, 2020, Ahmad *et al.*, 2020), the governing equations for the flow takes the form:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = u_e \frac{du_e}{dx} + \frac{1}{\rho_{hnf}} \frac{\partial}{\partial y} \left(\mu(T)\frac{\partial u}{\partial y}\right) - \frac{\sigma_{hnf}B^2(x)}{\rho_{hnf}}(u - u_e)$$
(2)

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \frac{1}{\left(\rho C_p\right)_{hnf}} \frac{\partial}{\partial y} \left[k(T)\frac{\partial T}{\partial y} \right] + \beta k_r^2 (T - T_\infty) \left(\frac{T}{T_\infty}\right)^n e^{\left(\frac{-E_a}{k_0 T}\right)} - \frac{1}{\left(\rho C_p\right)_{hnf}} \frac{\partial q_r}{\partial y} \tag{3}$$

$$u\frac{\partial C}{\partial x} + v\frac{\partial C}{\partial y} = D_B \frac{\partial^2 C}{\partial y^2} - k_r^2 (C - C_\infty) \left(\frac{T}{T_\infty}\right)^n e^{\left(\frac{-E_a}{k_0 T}\right)}$$
(4)

Subject to the following boundary conditions

$$u = u_w = \delta U_o x, v = 0, \ T = T_w, \ C = C_w \ , \quad at \ y = 0$$
$$u \to u_e = U_0 x, T \to T_\infty, C \to C_\infty, \qquad as \ y \to \infty$$
(5)

where the component of velocity for x and y axes are u and v respectively, u_e denotes the free stream velocity, δ is the parameter for plate velocity, *B*epitomizes the magnetic parameter, β is the exothermic parameter, *k*outlooks the thermal conductivity, q_r represents the radiative heat flux, k_r is the chemical reaction rate constant, T_{∞} symbolizes the free stream temperature, T_w is the wall temperature, D_B stands for the diffusion coefficient, C_{∞} is the ambient fluid concentration while C_w is the concentration at the wall and $\left(\frac{T}{T_{\infty}}\right)^n e^{\left(\frac{-Ea}{k_0T}\right)}$ denotes the Arrhenius function. Furthermore, the density of hybrid nanofluid ρ_{hnf} , viscosity of hybrid nanofluid μ_{hnf} , heat capacity of hybrid nanofluid $\left(\rho C_p\right)_{hnf}$, thermal conductivity of hybrid nanofluid K_{hnf} are as follow (Hayat and Nadeem 2017, Jawad *et al.*, 2021) and that of relevant nanomaterials are in table 1:

$$\rho_{hnf} = (1 - \omega_2) [(1 - \omega_1)\rho_f + \omega_1 \rho_{s1}] + \omega_2 \rho_{s2}, \qquad \mu_{hnf} = \frac{\mu_f}{(1 - \omega_1)^{2.5}(1 - \omega_2)^{2.5}},$$

$$(\rho C_p)_{hnf} = (1 - \omega_2) [(1 - \omega_1)(\rho C_p)_f + \omega_1(\rho C_p)_{s1}] + \omega_2 (\rho C_p)_{s2},$$

$$\sigma_{hnf} = \frac{2\sigma_{nf} + \sigma_{s2} - 2\omega_2(\sigma_{nf} - \sigma_{s_2})}{2\sigma_{nf} + \sigma_{s2} + \omega_2(\sigma_{nf} - \sigma_{s_2})} \times \frac{\sigma_{s1} + 2\sigma_f - 2\omega_1(\sigma_f - \sigma_{s1})}{\sigma_{s1} + 2\sigma_f + \omega_1(\sigma_f - \sigma_{s1})} \times \sigma_f$$

$$K_{hnf} = \frac{k_{s2} + 2k_{nf} - 2\omega_2(k_{nf} - k_{s2})}{k_{s2} + 2k_{nf} + \omega_2(k_{nf} - k_{s2})} \times \frac{k_{s1} + 2k_f - 2\omega_1(k_f - k_{s1})}{k_{s1} + 2k_f + \omega_1(k_f - k_{s1})} \times k_f,$$
(6)

where $\rho_{s1}, \omega_1, \sigma_{s1}, (\rho C_p)_{s1}, k_{s1}$ are the thermophysical properties for Al_2O_3 nanoparticle, $\rho_{s2}, \sigma_{s2}, \omega_2, (\rho C_p)_{s2}, k_{s2}$ are the thermophysical properties for silver nanoparticle, $\rho_f, \mu_f, \sigma_f, (\rho C_p)_f, k_f$ are the thermophysical properties for the base fluid.

The Roseland approximation for radiation (Zaib et al., 2018) is given as:

$$q_r = -\frac{4\sigma^*}{3k^*}\frac{\partial T^4}{\partial y}(7)$$

This is solved using Taylor's series and higher order terms neglecting higher order terms, thus the radiation term in equation (3) gives

Table 1: Thermophysical Properties of some nanofluids (Mekheimeret al., 2018; Khan etal. 2020)

Material	Density ρ (kg/m^3)	Specific Heat Capacity $C_p(J/KgK)$	Electrical Conductivity $\sigma(S/m)$	Thermal Conductivity K(W/mk)
Water	977	4180	2.1×10^{-4}	0.607
Silver (<i>Ag</i>)	10500	235	18.9	429
Aluminium Oxide (Al_2O_3)	3690	773	0.85×10^{-5}	40

$$\frac{\partial q_r}{\partial y} = \left(-\frac{16\sigma^* T_{\infty}^3}{3k_1} \frac{\partial^2 T}{\partial y^2} \right) \tag{8}$$

Introducing well established variables [Shehzard*et al.*, 2015; Mohammed *et al.*,2016; Prasad *et al.* 2010; Animasaun 2015, Ajayi et al, 2017] of the form

$$\theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}, \qquad \phi(\eta) = \frac{C - C_{\infty}}{C_w - C_{\infty}}, \\ \psi = \sqrt{\vartheta U_0} x f(\eta), \quad \eta = y \sqrt{\frac{U_0}{\vartheta}}, \qquad u = \frac{\partial \psi}{\partial y}, \\ v = \frac{\partial \psi}{\partial x} \tag{9}$$

In addition, the fluid viscosity and thermal conductivity are taken to be linear utility of temperature in the form

$$\mu(T) = \mu^* [1 + b(T_w - T)], k = K [1 + \gamma(T - T_\infty)]$$
(10)

Juxtaposing equations (1) - (5) with variables(8) - (10), the continuity equation (1) is automatically satisfied and the other equations reduces to the form:

$$\begin{bmatrix} (a + (1 - \theta)\xi) \\ (1 - \omega_{1})^{2.5}(1 - \omega_{2})^{2.5} \left\{ (1 - \omega_{2}) \left[(1 - \omega_{1}) + \frac{\omega_{1}\rho_{s_{1}}}{\rho_{f}} \right] + \frac{\omega_{2}\rho_{s_{2}}}{\rho_{f}} \right\} \frac{d^{3}f}{d\eta^{3}} \\
- \frac{\xi}{(1 - \omega_{1})^{2.5}(1 - \omega_{2})^{2.5} \left\{ (1 - \omega_{2}) \left[(1 - \omega_{1}) + \frac{\omega_{1}\rho_{s_{1}}}{\rho_{f}} \right] + \frac{\omega_{2}\rho_{s_{2}}}{\rho_{f}} \right\} \frac{d^{2}f}{d\eta^{2}} \frac{d\theta}{d\eta}}{d\eta} \\
- \frac{df}{d\eta} \frac{df}{d\eta} + f(\eta) \frac{d^{2}f}{d\eta^{2}} + 1 - \frac{H_{a}}{\left\{ (1 - \omega_{2}) \left[(1 - \omega_{1}) + \frac{\omega_{1}\rho_{s_{1}}}{\rho_{f}} \right] + \frac{\omega_{2}\rho_{s_{2}}}{\rho_{f}} \right\}} \left(\frac{df}{d\eta} - 1 \right) = 0 \quad (11) \\
\frac{3R_{a}(1 + \theta\epsilon) + 4}{3R_{a} \left[(1 - \omega_{2}) \left[(1 - \omega_{1}) + \frac{\omega_{1}(\rho C_{p})_{s_{1}}}{(\rho C_{p})_{f}} \right] + \frac{\omega_{2}(\rho C_{p})_{s_{2}}}{(\rho C_{p})_{f}} \right] \frac{d^{2}\theta}{d\eta^{2}} + P_{r}f(\eta) \frac{d\theta}{d\eta} + \\
\frac{\epsilon}{\left[(1 - \omega_{2}) \left[(1 - \omega_{1}) + \frac{\omega_{1}(\rho C_{p})_{s_{1}}}{(\rho C_{p})_{f}} \right] + \frac{\omega_{2}(\rho C_{p})_{s_{2}}}{(\rho C_{p})_{f}} \frac{d\theta}{d\eta} \frac{d\theta}{d\eta} + P_{r}\beta C_{r}\theta (1 + T_{d}\theta)^{n} e^{\left(\frac{-\varepsilon_{1}}{(1 + T_{d}\theta)}\right)} = 0 \quad (12)$$

$$\frac{d^2\phi}{d\eta^2} + S_c f(\eta) \frac{d\phi}{d\eta} - S_c C_r \phi (1 + T_d \theta)^n e^{\left(\frac{-E_1}{(1 + T_d \theta)}\right)} = 0$$
(13)

Subject to the boundary conditions

$$\frac{df(0)}{d\eta} = \delta, \quad f(0) = 0, \quad \theta(0) = 1, \quad \phi(0) = 1$$
$$\frac{df(\infty)}{d\eta} \to 1 \qquad \theta(\infty) \to 0, \qquad \phi(\infty) \to 0 \text{ (14)}$$

Where Chemical reaction parameter $C_r = \frac{k_r^2}{U_0}$, activation energy parameter $E_1 = \frac{E_a}{k_0 T_{\infty}}$, Local magnetic parameter $H_a = \frac{\sigma B^2}{\rho_f U_0}$, Temperature dependent thermal conductivity parameter $\epsilon = \gamma (T_w - T_{\infty})$, Temperature dependent viscosity parameter $\xi = b(T_w - T_{\infty})$, Schmidt number $S_c = \frac{\vartheta}{D_B}$, Prandtl number $P_r = \frac{(\rho C_p)_f \vartheta}{K_f}$, Radiation parameter $R_a = \frac{k_f k_1}{4\sigma^* T_{\infty}^3}$, temperature difference parameter $T_d = \frac{(T_w - T_{\infty})}{T_{\infty}}$. The physical qualities of engineering interest in this study are the skin friction coefficient c_f , local Nusselt number Nu_f and Sherwood number S_h which are defined as

$$C_f = \frac{\tau_w}{\rho_f U^2} , Nu_x = \frac{xq_w}{k_f (T_w - T_\infty)}, Sh = \frac{xJ_w}{D(C_w - C_\infty)}$$
(15)

and
$$\tau_w = \mu_{hnf} \left(\frac{\partial u}{\partial y}\right)_{y=0}$$
, $q_w = -k_{hnf} \left(\frac{\partial T}{\partial y}\right)_{y=0} + (q_r)_{y=0}$, $J_w = -D_B \left(\frac{\partial C}{\partial y}\right)_{y=0}$ (16)

3. Numerical Solution

The coupled ordinary differential equations (11) - (13) and their corresponding boundary conditions (14) are first reduced to a system of first order equations using the method of superimposition (Na, 1979) using the identities:

$$f = f_1, \frac{df}{d\eta} = f_2, \frac{d^2 f}{d\eta^2} = f_3, \theta = f_4, \frac{d\theta}{d\eta} = \theta' = f_5, \frac{d^2 \theta}{d\eta^2} = f_5', \phi = f_6, \frac{d\phi}{d\eta} = f_6', \frac{d^2 \phi}{d\eta^2} = f_7$$
(17)

The obtained system of equations are thereafter solved numerically using a finite difference like collocation code inMatlab bvp5c o.d.e. solver.

4. Results and Discussion

Numerical computation has been carried out for various values of activation energy parameter (E_1) , Chemical (C_r) ,Hartmann number(H_a), Schmidt reaction parameter number $(S_c),$ Prandtl number (P_r) , Radiation parameter (R), temperature difference parameter (T_d) , thermal conductivity parameter (ϵ) , velocity parameter (δ) and volume fraction parameter (ω)using the numerical scheme discussed in the previous section. The numerical values obtained from the result are plotted in Figures 2 –11 for $\beta = 0.2$, $P_r =$ $0.7, \delta = 0.4, \ Cr = 1; \ \beta = 0.2, \xi = 0.7, \ \epsilon = 0.7, \ Pr = 0.7, \ Ra = 1, \ H_a = 1, S_c = 0.22, \ Td = 0.7, \ E_1 = 0.7, \ E_2 = 0.7, \ E_3 = 0.7, \ E_4 = 0.7, \ E_5 = 0.22, \ Td =$ 1, n = 1 except otherwise stated. Figure 2 illuminates the variation in temperature instigated by a change in thermal conductivity parameter. The figure revealed that temperature increase as thermal conductivity



Figure 2: Variation in Thermal conductivity parameter with Temperature



Figure 3: Variation in Radiation parameter with Temperature

parameter increases. This observation is in harmony with Figure 6 reported by Hazarika and Konch Jadav (2014). Figure 3 illustrates the effect of radiation parameter on temperature. The figure demonstrated that radiation causes a drop in temperature. This behavior is in harmony with Figure 7 reported by Abdul Maleque (2013). The effect of Arrhenius parameter (E_1) on fluid heat sensation is elucidated in Figure 4. It can be noted that the Arrhenius parameter leads to a decline in temperature.

Figure 5 shows the influence of temperature difference on concentration profile. The figure showed that fluid concentration reduces for increase in temperature difference.

Effect of chemical reaction parameter on temperature is elucidated in Figure 6. The figure demonstrated that chemical reaction spark a rise in fluid temperature. This behavior is in harmony with Figure 21 reported by Animasaun (2015). The impact of chemical reaction parameter on concentration is demonstrated in Figure 7.



Figure 4: Variation in Arrhenius parameter(E_1) with Temperature



Figure 5: Variation in temperature difference parameter(T_d) with concentration



Figure 6: Variation in Chemical Reaction parameter (C_r) with Temperature



Figure 7: Variation in Chemical Reaction parameter (C_r) with Concentration



Figure 8: Variation in Exothemic parameter (β) with Temperature



Figure 9: Variation in velocity parameter (δ) with velocity



Figure 10: Variation in velocity parameter (δ) with Temperature



Figure 11: EffectofPrandtl number on Temperature

Concentration profile is a decreasing function of chemical reaction. This is in accord with Figure 20 by Animasaun (2015). The variation in exothermic parameter with temperature is shown in Figure 8. The figure illuminated that temperature increases with exothermic parameter. This behavior is due to the fact that in exothermic reaction heat is released and so by increasing this parameter means more of such reaction which commulates to more heat into the system. Impact of Velocity parameter on velocity profile is shown in figure 9. The figure pictured fluid velocity as an increasing function of velocity parameter. The underlining reason for this behavior is due to the fact that the velocity parameter is a direct function of the plate velocity and as such, increasing this parameter translate to increasing plate velocity which will invariably enhance fluid flow. Figure 10 elucidated the variation of velocity parameter with temperature and the figure revealed that the parameter causes a decline in fluid temperature.

Figure 11 portrayed the impact that Prandtl number parameter have on fluid temperature. The figure displayed that temperature reduces for rising Prandtl number and this is because Prandl number is inversely proportionaly to fluid thermal conductivity while thermal conductivity is a direct function of temperature, hence the resulting decrease in temperature. In each of the figures, the influence of selected parameters where comparatively shown for both Al_2O_3 nanofluid and the hybrid version($Ag - Al_2O_3$). The hybrid version showed better response to variations in parameters in most of these figures.

6.Conclusion

The analysis of various parameters for the steady laminar forced convection flow of an incompressible, electrically conducting hybrid nanofluid has been carried out. The following were detected:

- i. Velocity parameter enhances fluid flow but causes a decline in fluid temperature.
- ii. Fluid temperature increases for a rise in any of thermal conductivity, chemical reaction and exothermic constraints while a decline is experienced due to radiation, velocity parameter, Prandtl number and Arrhenius parameter.
- iii. Concentration distribution is a decreasing function of each chemical reaction and temperature difference.
- iv. The hybrid duo of $Ag Al_2O_3$ shows better respose to variation in parameters than a single nano item.

v. Thermal conductivity parameter and the Prandtl number cause a rise in the Nusselt number whilePrandtl number reduces Sherwood number.

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